Answers - Point Source Lab

Calculating Hourly Emissions of SO_2 $E_{SO2} = (C \times MW \times Q \times 60)$

 $(V \times 10^6)$

$$E_{SO2} = 1,058.8 \times 64 \times 155,272 \times 60 = 1,637 \text{ lb/hr}$$

 385.5×10^6

Calculating Heat Input

$$H_{in} = (Q_{\underline{f}} \times HHV)$$

$$(10^6)$$

$$H_{in} = 46,000 \times 18,000 = 828 \text{ MMBtu/hr}$$
 10^6

Developing SO₂ Emission Factors

$$EF_{SO2} = E_{SO2} = 1,637 \text{ lb/hr} = 1.98 \text{ lb/MMBtu}$$
 $H_{in} = 828 \text{ MMBtu/hr}$

Calculating Annual SO2 Emissions

Annual SO₂ Emissions = Hourly SO₂ emissions x Op Hrs

= (1,637 lb/hr x 5,400 hrs) = 4,419 tons per year(2,000 lb/ton)

Calculation 2. Boiler Emissions (Source Testing)

 P_b Emission Rate = P_b concentration x stack gas flow rate

- $= 0.0005 \text{ lb/dscf} \times 51,700 \text{ dscf/min} \times 60 \text{ min/hr}$
- = 1,551 lb/hr

Annual P_b Emissions = 1,551 lb/hr x 5,840 hr/yr x 1 ton/2,000 lb = 4,528 tpy

Calculation 3. Copper Coil Manufacturing (Mass Balance)

Consumption = (mass of coil and oil to annealer - mass of coil processed) x 85 percent

 $= (5,075 \text{ kg} - 5,000 \text{ kg}) \times 0.85$

= 64 kg oil destroyed in the annealer

Calculation 3. Copper Coil Manufacturing (Mass Balance)

Estimate of Output (emissions)

Output = Input - Consumption - Accumulation

- = 3,000 kg 64 kg 2,800 kg
- = 136 kg

The VOC emissions associated with this process are thus 136 kg oil pr 5,000 kg of copper coil process, or 0.027 kg oil per kg of copper coil processed.

Calculation 4. Boiler Emissions (Fuel Analysis)

 $E_{SO2} = Q_f x$ pollutant concentration in fuel x (MW_p/MW_f)

- $= 5,000 \text{ lb/hr} \times 0.01 \times (64/32)$
- = 100 lb/hr
- = 100 lb/hr x 8,760 hr/hr x <u>1 ton</u> 2,000 lbs
- $= 438 \text{ tons/year of SO}_2$

- Boiler Emissions = Annual Coal Consumption x Emission Factor
- TOC = 928,000 tons/year x 0.3 lb/ton = 278,400 lb/year = 139.2 tpy
- $P_b = 928,000 \text{ tons/year x } 8.9E-03 \text{ lb/ton} = 8,259 \text{ lb/year}$ = 4.1 tpy
- $NO_x = 928,000 \text{ tons/year x 9 lb/ton} = 8,352,000 \text{ lb/year}$ = 4,176 tpy
- CO = 928,000 tons/year x 0.6 lb/ton = 556,800 lb/year = 278 tpy

Estimating Uncontrolled Emissions for SO₂
SO₂ Emissions = Annual Coal Consumption x
(Emission Factor x Coal Sulfur Content)

- = 928,000 tons/year x (39 lb/ton x 1.87) = 67,679,040 lb/year
- = 33,840 tpy

Estimating Controlled Emissions

Controlled Emissions = Uncontrolled Emissions x (1 - Efficiency/100)

Total PM = 2,858 tpy x
$$(1-75/100) = 2,858$$
 tpy x $(0.25) = 715$ tpy

$$SO2 = 33,840 \text{ tpy x } (1-93/100) = 33,840 \text{ tpy x}$$

 $(0.07) = 2,369 \text{ tpy}$

Temporal Allocation

Seasonal emissions = Seasonal throughput fraction x annual emissions

Winter PM = $0.5 \times 715 \text{ tpy} = 357.5 \text{ tons}$

Spring $PM = 0.2 \times 715 \text{ tpy} = 143 \text{ tons}$

Summer $PM = 0.1 \times 715 \text{ tpy} = 715 \text{ tons}$

Fall PM = $0.2 \times 715 \text{ tpy} = 143 \text{ tons}$

Answers - Area Source Lab

Calculation 1. Estimating County Level Wood Usage (Top-Down Approach)

County Wood Use = State wood use x county households/state households

= 622,000 x 1,242/80,047 = 9,651 cords burned in county of study

Calculation 1. Estimating County Level Wood Usage (Top-Down Approach)

- Total waste generated = Total number of households using burn barrels x average waste generated per household
- $= 997 \times 6.75 = 6{,}730 \text{ lb/day}$
- Total Combustible waste generated by households
 - = Total waste generated x percentage of combustible waste
- = 6,730 lb/ day x 80/100 = 5,384 lb/day
- Total combustible waste = 5,384 lb/day = 2.69 ton/day

Calculation 1. Estimating County Level Wood Usage (Top-Down Approach)

Daily Emissions = Emission Factor

x Total Combustible waste generated (in tons)

CO = 85 lb/ton x 2.69 tons/day = 228.6 lb/day

PM = 16 lb/ton x 2.69 tons/day = 43.03 lb/day

SOx = 1 lb/ton x 2.69 tons/day = 2.69 lb/day

NOx = 6 lb/ton x 2.69 tons/day = 16.14 lb/day

TOC = 21.5 lb/ton x 2.69 tons/day = 57.84 lb/day

TOC = Total organic compound

Calculation 3. State I Gasoline Marketing (Rule Effectiveness/Rule Penetration

Calculating Emissions

```
E = A \times EF \times 1 - (CE \times RE \times RP)
```

- $= 500 \times 11.5 \times 1 ((0.95)(0.8)(0.93))$
- = 1,685 lb of VOC/day

Calculation 4. Surface Coating Operations (Mass Balances)

Estimating Uncontrolled PM Emissions

- Coating density of solid content = Density of coating A Density of volatile content
- = 7.5 lb/gal 6.2 lb/gal = 1.3 lb solids/gal
- Uncontrolled PM emissions = Density of solid content x annual usage x (1-transfer efficiency)
- = 1.3 lb/gal x 1,600 gal/yr x (1 0.6)
- = 832 lb/yr or 0.416 tpy

Calculation 4. Surface Coating Operations (Mass Balances)

Estimating Controlled PM Emissions

Controlled PM Emissions = Uncontrolled PM x (1 - Control efficiency)

= 0.416 x (1 - 99/100) = 0.00416 tpy of solids

Calculation 5. Surface Coating (Per Employee Emission Factor)

Calculating Area Source Emissions

- VOC emissions from area sources = area source employment x average coating usage x % VOC x coating density
- = 900 employees x 12 gal/yr x 7.5 lb/gal x 45/100
- = 36,450 lb/yr
- = 18.23 tpy of VOC

Calculation 6. Emissions from Benzene Loading Operations (Emission Factor)

$$L_{L} = 12.46 \text{ x } \underline{S \text{ x P x M}}$$

$$T$$

$$L_{L} \text{ (lb/103 gal)} = \underline{12.46 \text{ x } 0.6 \text{ x } 2 \text{ psia x } 78} \frac{\text{lb}}{\text{lb - Mole}}$$

$$\underline{540^{\circ} \text{ R}}$$

= 2.16 lb benzene/1,000 gal

Toxics Lab

Example Calculation #1

Actual Annual and Potential Acetaldehyde Uncontrolled Emissions from a Natural Gas-Fired Heater

Given: Actual hours of operation = 2400 hr/yr at 80% of maximum capacity

Heat content = 1050 MMBtu/MMCF

Heat input rate = 2 MMBtu/hr

Acetaldehyde emission factor for commercial-sized heater (see NTI

documentation) = 1.3 E-08 lb acetaldehyde/MM Btu

Example Calculation #1 (Continued)

Actual Acet emissions($\frac{\text{lb}}{\text{yr}}$) = (*EF*)(*heat* input rate)(annual operation)(% firing capacity)

where:

EF = pollutant emission factor in lb/MMBtu and heat input rate = maximum firing rate in MMBtu/hr.

Example Calculation #1 (Continued)

Actual Emissions = $(1.3x10-8 \frac{1b}{MMBtu})(2\frac{MMBtu}{hr})(2400\frac{hr}{yr})(80\%)$

Potential Emissions = $(1.3x10 - 8\frac{1b}{MMBtu})(2\frac{MMBtu}{hr})(2400\frac{hr}{yr})(100\%)$

Actual Emissions = $4.99 \times 10-5 \text{ lb/yr}$

Potential Emissions = $6.24 \times 10-5 \text{ lb/yr}$

Example Calculation #2

Uncontrolled Actual Annual and Potential Xylene Emissions from a Silk Screen Printing Process

Given:

Constituents of ink thinner (100% VOC by weight, 5% xylene by weight)

Usage of ink thinner = 45 *lb/yr*

Constituents of ink (10% VOC by weight, 2% xylene by weight)

 $Usage\ of\ ink = 204\ lb/yr$

Estimated maximum hourly usage = 1 lb ink and 0.3 lb thinner

Example Calculation #2 (Continued)

Actual xylene
$$\left(\frac{lb}{yr}\right) = \left[\left(\left(45\frac{lb}{yr}\right)\left(0.05\frac{lb xylene}{lb}\right)\right) + \left(\left(204\frac{lb}{yr}\right)\left(0.02\frac{lb xylene}{lb}\right)\right)\right]$$

$$= 6.33\frac{lb xylene}{yr}$$

Potential xylene
$$\left(\frac{lb}{yr}\right) = \left[\left(\left(0.3 \frac{lb}{hr}\right)\left(0.05 \frac{lb \text{ xylene}}{lb}\right)\right) + \left(\left(1 \frac{lb}{hr}\right)\left(0.02 \frac{lb \text{ xylene}}{lb}\right)\right)\right] * 8760 \frac{hr}{yr}$$

$$=307 \frac{\text{lb xylene}}{\text{yr}}$$

Example Calculation #3

Cr(VI) Emissions from a Surface Coating Operation

Given: Coating usage = 500 gal/year

Cr(VI) concentration = 0.08% Cr(VI), by mass

Density = 8 lb/gal

Coating transfer efficiency = 40%

Air pollution control device = 80%

Example Calculation #3 (Continued)

$$E_{x} = (Q_{in} - Q_{out}) * C_{x}$$

Where: E_x = Total emissions of pollutant x

Q_{in} = Quantity of material entering the process

Q_{out} = Quantity of material leaving the process as waste, recovered, or in product

 C_x = Concentration of pollutant x

Example Calculation #3 (Continued)

Mass of Cr(VI) entering spray booth:

=
$$500 \text{ gal/yr} \times 8 \text{ lb/gal} \times .0008 \text{ lb } \text{Cr(VI)/lb coating}$$

= 3.2 lb/yr

Mass of Cr(VI) removed from spray booth:

From transfer to surface

$$3.2 \times 0.4 = 1.28$$
 lbs/yr

Leaving 1.92 lb/yr

From air pollution control device

$$1.92 \times 0.8 = 1.54 \text{ lb/yr}$$

Example Calculation #3 (Continued)

Emission rate =
$$3.2 lb/yr - 1.28 lb/yr - 1.54 lb/yr$$

= $0.38 lb/yr$

or

Emission rate =
$$3.2 \text{ lb/yr } x (1-0.4) x (1-0.8)$$

= 0.38 lb/yr